

1258527

TO AND TWO WITNESSES IN PRESENCE STATED, WHEREAS,

UNITED STATES DEPARTMENT OF COMMERCE

United States Patent and Trademark Office

December 09, 2004

THIS IS TO CERTIFY THAT ANNEXED HERETO IS A TRUE COPY FROM
THE RECORDS OF THE UNITED STATES PATENT AND TRADEMARK
OFFICE OF THOSE PAPERS OF THE BELOW IDENTIFIED PATENT
APPLICATION THAT MET THE REQUIREMENTS TO BE GRANTED A
FILING DATE.

APPLICATION NUMBER: 60/525,549
FILING DATE: *November 26, 2003*
RELATED PCT APPLICATION NUMBER: PCT/US04/34236

Certified by

Jon W Dudas

Acting Under Secretary of Commerce
for Intellectual Property
and Acting Director of the U.S.
Patent and Trademark Office



Please type a plus sign (+) inside this box →

PTO/SB/16 (5-03)

Approved for use through 04/30/2003. OMB 0651-0030

U.S. Patent and Trademark Office; U.S. DEPARTMENT OF COMMERCE

Under the Paperwork Reduction Act of 1995, no persons are required to respond to a collection of information unless it displays a valid OMB control number.

1785 U.S.P.T.O.
601525349
112603

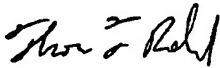
PROVISIONAL APPLICATION FOR PATENT COVER SHEET

This is a request for filing a PROVISIONAL APPLICATION FOR PATENT under 37 CFR 1.53(c).

INVENTOR(S)		
Given Name (first and middle [if any])	Family Name or Surname	Residence (City and either State or Foreign Country)
Scott Peter Noah Oliver	SCHMIDT CALLAIS MACY GUERRET	Limerick, PA Collegeville, PA Royersford, PA Mazerolles, France
<input type="checkbox"/> Additional inventors are being named on the _____ separately numbered sheets attached hereto		
TITLE OF THE INVENTION (280 characters max) CONTROLLED RADICAL ACRYLIC COPOLYMER THICKENERS		
Direct all correspondence to: CORRESPONDENCE ADDRESS		
<input type="checkbox"/> Customer Number	<input type="text"/>	<input type="checkbox"/> Place Customer Number Bar Code Label here
OR	Type Customer Number here	
<input checked="" type="checkbox"/> Firm or Individual Name	Thomas F. Roland, Esq.	
Address	ATOFINA Chemicals, Inc.	
Address	2000 Market Street, 26th Floor	
City	Philadelphia	State PA ZIP 19103
Country	USA	Telephone 215-419-7314 Fax 215-419-7075
ENCLOSED APPLICATION PARTS (check all that apply)		
<input checked="" type="checkbox"/> Specification	Number of Pages 31	<input type="checkbox"/> CD(s), Number
<input checked="" type="checkbox"/> Drawing(s)	Number of Sheets 2	<input checked="" type="checkbox"/> Other (specify) Claims-2 pages, Abstract-1 page
<input type="checkbox"/> Application Data Sheet. See 37 CFR 1.76		
METHOD OF PAYMENT OF FILING FEES FOR THIS PROVISIONAL APPLICATION FOR PATENT (check one)		
<input type="checkbox"/> A check or money order is enclosed to cover the filing fees	FILING FEE	
<input checked="" type="checkbox"/> The Director is hereby authorized to charge filing fees or credit any overpayment to Deposit Account Number 01-2717	AMOUNT (\$)	
<input type="checkbox"/> Payment by credit card. Form PTO-2038 is attached.	\$160.00	
The invention was made by an agency of the United States Government or under a contract with an agency of the United States Government.		
<input checked="" type="checkbox"/> No.		
<input type="checkbox"/> Yes, the name of the U.S. Government agency and the Government contract number are: _____		

Respectfully submitted,

SIGNATURE



Date

11-26-03

TYPED or PRINTED NAME Thomas F. Roland, Esquire

215-419-7314

REGISTRATION NO.

42,110

(if appropriate)

Docket Number:

IR 3725 PSP

TELEPHONE

USE ONLY FOR FILING A PROVISIONAL APPLICATION FOR PATENT

This collection of information is required by 37 CFR 1.51. The information is used by the public to file (and by the PTO to process) a provisional application. Confidentiality is governed by 35 U.S.C. 122 and 37 CFR 1.14. This collection is estimated to take 8 hours to complete, including gathering, preparing, and submitting the complete provisional application to the PTO. Time will vary depending upon the individual case. Any comments on the amount of time you require to complete this form and/or suggestions for reducing this burden, should be sent to the Chief Information Officer, U.S. Patent and Trademark Office, U.S. Department of Commerce, P.O. Box 1450, Alexandria, VA 22313-1450. DO NOT SEND FEES OR COMPLETED FORMS TO THIS ADDRESS. SEND TO: Mail Stop Provisional Application, Commissioner for Patents, P.O. Box 1450, Alexandria, VA 22313-1450.

CERTIFICATE OF MAILING BY "EXPRESS MAIL" (37 CFR 1.10)

Applicant(s):

Docket No.

IR 3725 PSP

Serial No.
Not yet assignedFiling Date
herewithExaminer
Not yet assignedGroup Art Unit
Not yet assignedInvention: **CONTROLLED RADICAL ACRYLIC COPOLYMER THICKENERS**

I hereby certify that the following correspondence:

Provisional Application Cover Sheet, Certificate of Express mailing; and Provisional Application*(Identify type of correspondence)*

is being deposited with the United States Postal Service "Express Mail Post Office to Addressee" service under 37 CFR 1.10 in an envelope addressed to: Commissioner for Patents, P.O. Box 1450, Alexandria, VA 22313-1450 on

November 26, 2003*(Date)*Meleah J. Scott*(Typed or Printed Name of Person Mailing Correspondence)**(Signature of Person Mailing Correspondence)*EV 269963450 US*("Express Mail" Mailing Label Number)***Note: Each paper must have its own certificate of mailing.**

CONTROLLED RADICAL ACRYLIC COPOLYMER THICKENERS

5

Field Of the Invention

The present invention relates to acrylic block copolymers synthesized by a controlled free-radical process, and their use as additives and thickeners in oil-based compositions. They are especially useful as viscosity index improvers in lubricating 10 oil.

Background of the Invention

Lubricating oils, such as motor oils, gear oils, hydraulic fluids and transmission fluids typically contain several additives to improve their performance. 15 These can include dispersants, antioxidants, detergents, friction modifiers, de-foaming agents, pour-point depressants, and viscosity index improvers.

The viscosities of lubricating oils are temperature dependent, thus as the temperature of the oil is increased the viscosity typically decreases, and conversely as the temperature of an oil decreases the viscosity will increase. A significant loss of 20 viscosity can be detrimental as it may cause the oil to flow more quickly off of the metal parts it is designed to protect. A viscosity index improver (VII) is typically a polymeric material, which principally functions by minimizing the viscosity variations over a wide range of temperatures. Normally these are used to reduce the viscosity loss of lubricating oils upon heating.

25 Random copolymers are commonly used as VII's. To ensure solubility in a lubricating oil base, these copolymers are formed from at least one monomer whose homopolymer is oil-soluble. Three types of random copolymers commonly used as

VIIIs are: polymethacrylates (US 6,124,249), olefinic copolymers (US 2003/0073785), and conjugated dienes (US 6,319,881).

Polymers having a controlled architecture, including star copolymers (EP 1064347) and block copolymers have been described in the art. These polymers can
5 be prepared through a variety of living anionic and living (or controlled) free radical polymerization techniques. These techniques have been used primarily to control the molecular weight distribution.

US 6,538,091 describes a process for the control of a polymer architecture using an atom transfer process (ATRP) based on a redox reaction with a transition
10 metal compound. This process uses an initiating system resulting in a copolymer having a predictable molecular weight and a controlled polydispersity. Polymers made by the process are described as useful for molding materials, barrier materials, thermoplastic elastomers, and amphiphilic surfactants. This controlled radical polymerization technique has several drawbacks such as, residual metallic by-
15 products which can be detrimental to many applications (for example see US 6,610,802) and limitations in polymer composition. Furthermore, the reference does not describe the use of any of the copolymers in lubricating oils.

Random copolymers made by ATRP have been used as pour point depressants (US 6,391,996), and viscosity index improvers (US2002/0188081). The '081
20 reference mentions that the ATRP process could be used for blocky copolymers, but fails to exemplify such a use, or recognize the large VII benefit of using such block copolymers in lubricating oils. Also, gradient copolymers synthesized by ATRP have been shown useful as pour point depressants in US 6,403,745. Again, the use of relatively high catalytic amounts of metal compounds leads to product containing
25 residual metal contamination. These metallic by-products are detrimental in engine-

type lubricant applications and require removal, which is difficult and requires laborious procedures.

The use of multifunctional lubricant additives has been described in US 6,319,881.

- 5 Block copolymers have also been shown to be useful as VIIIs. Block copolymers of a vinyl aromatic monomer and a vinyl aromatic-co-acrylic block prepared by stabilized free radical polymerization are described in patents EP 0 945 474, and US 6,531,547. These patents describe the use of TEMPO-based nitroxide derivatives for the synthesis of the corresponding block copolymers. This class of free
- 10 radical control agent does not provide control over acrylic type monomers.
- Specifically, the use of methacrylates as in the above example, will lead to side and termination reactions such as disproportionation, which inhibits the formation of block copolymers and long chain molecules (as described by Ananchenko et. al. in the *Journal of Polymer Science: Part A: Polymer Chemistry*, Vol. 40 pp 3264-3283).
- 15 Also, block copolymers of ethylene and alpha-olefins have been described in US 2003/0073785 and block copolymers of poly(conjugated dienes) and poly(monovinyl aromatic hydrocarbons have been described in US 6,303,550. None of the above references makes use of a controlled architecture copolymer having at least one pure acrylic block segment for use as a VII.
- 20 US 5,002,676 describes the preparation of block copolymers containing selectively hydrogenated conjugated dienes and *t*-butyl methacrylate. US 6,350,723 teaches the synthesis of block copolymers through the living anionic polymerization of a conjugated diene and an alkyl methacrylate monomer. These references exemplify the use of block copolymers containing conjugated dienes and hydrogenated dienes,
- 25 but fail to teach the specific copolymers of the present invention. Also these reports

do not teach the significance of tailoring block solubilities or allow for the formation of gradient compositions. Furthermore, living anionic polymerization suffers from several drawbacks, such as, ineffectiveness at temperatures above – 20 °C, poor copolymerization between polar and non-polar comonomers, and the inability to use

5 monomers that can be easily deprotanated. Therefore functional monomers cannot be incorporated, and the copolymerization of monomer mixtures can be problematic and/or unusable. Furthermore this process can be expensive and difficult or impractical to carry out on an industrial scale as bulk or emulsion techniques cannot be used, extremely pure reagents are necessary (even trace amounts of protic material

10 inhibits polymerization), and an inert atmosphere is requisite.

A process for preparing copolymers in the presence of a stable free radical from the nitroxide family is described in US 6,255,402. Nitroxide-mediated stable radicals have been used to produce controlled block copolymers, as described in US 6,255,448, and US 2002/0040117. These references, incorporated herein by

15 reference, do not describe the use of the copolymers in lubricating oils.

Surprisingly it has now been found that an acrylic block copolymer formed by a controlled-radical polymerization, produces excellent viscosity index improvement in lubricating oils. The polymers of the invention produce a greater VI improvement than found in random copolymers or other block copolymers currently used. While

20 the properties attained in traditional copolymers are typically an average of the properties imparted by the resultant monomers incorporated, block copolymers lead to a material containing the characteristic properties inherent to the parent homopolymers comprising each segment. Therefore, the use of block copolymers is particularly adventitious for the formation of materials containing multifunctional

25 properties. Furthermore, these polymers should provide enhanced shear stability due

to the controlled molecular weights and molecular weight distribution provided by the controlled polymerization process. The viscosity modifying advantages of these copolymers for lubricant oil applications can be exemplified by the excellent performance demonstrated in typical SAE Standard J300 viscosity classification

5 testing. Furthermore these block copolymers can be used to thicken any number of oil-based compositions.

Summary of the Invention

It is an objective of the invention to provide a controlled-architecture
10 copolymer capable of thickening oil-based compositions.

Another objective of the invention is to provide a lubricating oil with good
viscosity index improvement by utilizing an acrylic block copolymer.

It is a further objective of the invention to adjust the copolymer composition
and physical properties of a controlled-radical copolymer for the optimal viscosity
15 index improvement in a given lubricating oil.

It is also an objective of the invention to synthesize an acrylic block
copolymer by a nitroxide-mediated polymerization process.

It is still a further objective of the invention to provide an acrylic block
copolymer having multifunctional properties such as improved shear stability, pour
20 point depression, dispersant, etc..

These objectives have been met in a thickened oil composition comprising:

- a) from 99.999 to 60.0 weight percent of one or more oils, and
- b) from 0.001 to 40.0 weight percent of a controlled architecture
amphiphilic block copolymer having at least one acrylic block.

Brief Description of the Drawings

Figure 1 graphically illustrates the reduced viscosity versus the concentration of lubricating oils containing comparative VIIIs and VIIIs of the invention. The plot shows that the comparative VIIIs show a linear increase in reduced viscosity with increased concentration, while the VIIIs of the invention show a marked increase or divergent behavior in the reduced viscosity above a concentration of about 5 percent.

5 Figure 2 is an analogous plot to Figure 1, representing a block copolymer having about twice the Mn as compared to the block shown in Figure 1.

Figure 3 graphically illustrates the VI versus the weight percentage of polymer
10 incorporated in a lubricating oil composition containing comparative VIIIs and VIIIs of the invention. The plot indicates the VIIIs of the invention provide similar VII behavior at much lower weight percentages as compared to the comparative VIIIs.

Figure 4 is the same plot as Figure 4, rescaled for clarity.

15 **Detailed Description of the Invention**

The present invention is directed to oil-based compositions containing a controlled architecture block copolymer having at least one acrylic block. Preferably the block copolymer is amphiphilic. The term amphiphilic is meant to describe a block copolymer in which at least one block segment is readily soluble in an oil, and
20 one segment is partially or completely insoluble in the oil. The amphiphilic nature will of course be dependant on the nature of the oil. The specific composition of the corresponding block copolymers can be tailored accordingly based on the base oil utilized, to attain the desired amphiphilic behavior.

The Hildebrand solubility parameter can be used as a useful guide to
25 determine the solubility of polymers in a specific medium. A detailed summary of this

parameter is provided in the chapter entitled "Solubility Parameter Values", by E. A. Grulke in the *Polymer Handbook*, Fourth Edition, ed. J. Brandrup, E. J. Immergut, and E. A. Grulke, John Wiley & Sons, New York, 1999. Although the solubility parameters best describe nonpolar solvents, they have been extended to include both 5 polar solvents and polymeric materials as described in the *Polymer Handbook*, page VII/677. The solubility parameter of numerous commercial polymers as well as methods (both experimental and theoretical) for estimating the solubility parameter is also contained in the above stated reference. While the solubility of a particular polymer in a lubricating oil will be dependant on factors such as molecular weight, 10 temperature, and so forth, it is frequently found that polymers will dissolve in solvents having solubility parameters within about 1 to 1.5 units of their own (based on solubility parameters given in $(J/m^3)^{1/2}$). In order to definitively assess the solubility of a polymer segment in an oil, the corresponding homopolymer must be directly tested.

The compatibility of each segment can be estimated using Hildebrand 15 solubility parameters. The oil-soluble block typically has a solubility parameter within $2.0 (J/m^3)^{1/2}$ of the selected lubricating oil, preferably within $1.5 (J/m^3)^{1/2}$; and the oil-insoluble block has a solubility difference of greater than $1.5 (J/m^3)^{1/2}$, and preferably greater than $2.0 (J/m^3)^{1/2}$. Block copolymer compositions in which both segments are soluble in oil can be used, however this minimizes the ability to form micelles or 20 aggregates which can provide beneficial attributes to the system.

The block copolymers of the present invention find use, among other things, as thickeners or viscosity modifiers of oil-based formulations. Oils useful in the invention include, but are not limited to, mineral oils, synthetic oils, silicon oils, and lubricating oils. In one preferred case, these block copolymers may be solubilized in

base oils to form a lubricating oil composition. The oil makes up from 60 to 99.999 percent by weight of the oil composition, preferably from 80 to 99.99 percent.

Typical paraffinic lubricating oils have a solubility parameter of about 16 $(J/m^3)^{1/2}$, however the solubility parameter will fluctuate, depending on the 5 napthenic content along with other factors. Therefore, a "soluble" polymer block may be one with a solubility parameter of roughly 14-18 $(J/m^3)^{1/2}$. Examples of oil-compatible blocks that have a solubility parameter very similar to paraffinic oil include, but are not limited to polymers of dodecyl methacrylate, mixtures of C₁₆ to C₂₂ methacrylates, C₆ to C₃₀ linear or branched acrylates, methacrylates and mixtures 10 thereof. The oil insoluble blocks can be formed from one or more monomers resulting in a segment of desired solubility.

Examples of polymer blocks insoluble in paraffinic oil include, but are not limited to those formed from methyl acrylate, methyl methacrylate, polystyrene, methoxyethyl acrylate, polyethylene glycol methylether acrylate and methacrylate, C₁ 15 to C₃ methacrylates, C₁ to C₄ linear and branched acrylates, and mixtures thereof. A monomer forming an oil-soluble polymer can be copolymerized with a monomer forming an oil-soluble polymer in such a ratio that the resultant block segment is insoluble. It has been found that blocks of polymers having a solubility parameter of 19 $(J/m^3)^{1/2}$ or greater can be synthesized and exhibit exceptional viscosity index 20 improvement when used in the present invention.

By "copolymers" as used herein, is meant polymers formed from at least two chemically distinct monomers. The copolymer includes terpolymers and those polymers formed from more than three monomers. Each block segment may consist of a homopolymer, or may be a copolymer of two or more different monomers.

Block copolymers of the present invention are those formed by a controlled radical polymerization (CRP). They differ from random copolymers that may contain some blocks of certain monomers related either to a statistical distribution, or to the differences in reaction rates between the monomers. In these random

5 polymerizations, there is no control over the polymer architecture, molecular weight, or polydispersity and the relative composition of the individual polymer chains is non-uniform. Included as block copolymers of the present invention are diblock copolymers, triblock copolymers, multiblock copolymers, star polymers, comb polymers, gradient polymers, and other polymers having a blocky structure, which

10 will be known by those skilled in the art.

When a copolymer segment is synthesized using a CRP technique such as nitroxide-mediated polymerization, it is termed a gradient or ‘profiled’ copolymer. This type of copolymer is different than a polymer obtained by a traditional free radical process and will be dependant on the monomer composition, control agent,

15 and polymerization conditions. For example, when polymerizing a monomer mix by traditional free radical polymerizations, a statistical copolymer is produced, as the composition of the monomer mix remains static over the lifetime of the growing chain (approximately 1 second). Furthermore, due to the constant production of free radicals throughout the reaction, the composition of the chains will be non-uniform. During a

20 controlled radical polymerization the chains remain active throughout the polymerization, thus the composition is uniform and is dependant on the corresponding monomer mix with respect to the reaction time. Thus in a two monomer system where one monomer reacts faster than the other, the distribution or ‘profile’ of the monomer units will be such that one monomer unit is higher in

25 concentration at one end of the polymer segment.

The copolymers of the invention are acrylic block copolymers. By acrylic block copolymer, as used herein, is meant that at least one block of the copolymer is formed entirely or almost entirely from one or more acrylic monomers. The acrylic block contains at least 90 mole percent of acrylic monomer units, preferably at least 5 95 mole percent, and most preferably at least 98 mole percent. In one preferred embodiment, the acrylic block contains 100 percent acrylic monomer units. The other block or blocks may be acrylic or non-acrylic.

By "acrylic" as used herein is meant polymers or copolymers formed from acrylic monomers including, but not limited to, acrylic acids, esters of acrylic acids, 10 acrylic amides, and acrylonitriles. It also includes alkacryl derivatives, and especially methacryl derivative. Functional acrylic monomers are also included. Examples of useful acrylic monomers include, but are not limited to acrylic acid; methacrylic acid; alkyl esters and mixed esters of (meth)acrylic acid; acrylamide, methacrylamide, N- and N,N-substituted (meth)acrylamides, acrylonitrile, maleic acid, fumaric acid, 15 crotonic acid, itaconic acid and their corresponding anhydrides, carbonyl halides, amides, amidic acids, amidic esters, and the full and partial esters thereof. Especially preferred acrylic monomers include methyl acrylate, ethyl acrylate, butyl acrylate, and C₈-C₂₂ alkyl (meth)acrylates, and mixtures thereof.

The other block or blocks of the copolymer may be acrylic, or formed from 20 one or more non-acrylic ethylenically unsaturated monomers. In one preferred embodiment all blocks of the copolymer are acrylic blocks. Other ethylenically unsaturated monomers useful in the invention include, but are not limited to, anhydrides, vinyl esters, alpha-olefins, substituted or unsubstituted mono and dialkyl esters of unsaturated dicarboxylic acids, vinyl aromatics, cyclic monomers, monomers 25 containing alkoxylated side chains, sulfonated monomers, and vinyl amide monomers.

Acrylic monomers may also be used at any level. A combination of ethylenically unsaturated monomers may also be used. A preferred non-acrylic monomer is styrene.

In principle, any living or controlled polymerization technique can be utilized.

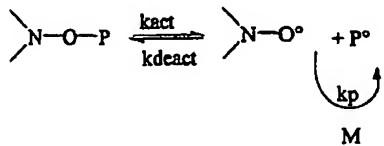
- 5 However, for the practicality of controlling acrylics, and creating copolymer segments of different polarities (including functional acrylics) the block copolymers of the present invention are preferably formed by controlled radical polymerization (CRP). These processes generally combine a typical free-radical initiator with a free radical stabilizing compound to control the polymerization process and produce polymers of
- 10 a specific composition, and having a controlled molecular weight and narrow molecular weight range. These free-radical initiators used may be those known in the art, including, but not limited to peroxy compounds, peroxides, hydroperoxides and azo compounds which decompose thermally to provide free radicals.

- Examples of controlled radical polymerization techniques will be evident to
- 15 those skilled in the art, and include, but are not limited to, atom transfer radical polymerization (ATRP), reversible addition fragmentation chain transfer polymerization (RAFT), nitroxide-mediated polymerization (NMP), boron-mediated polymerization, and catalytic chain transfer polymerization (CCT). Descriptions and comparisons of these types of polymerizations are described in the ACS Symposium Series 768 entitled *Controlled/Living Radical Polymerization: Progress in ATRP, NMP, and RAFT*, edited by Krzysztof Matyjaszewski, American Chemical Society, Washington, D.C., 2000.

- One preferred method of controlled radical polymerization is nitroxide-mediated CRP. Nitroxide-mediated polymerization can occur in bulk, solvent, and
- 25 aqueous polymerization, can be used in existing equipment at reaction times and

temperature similar to other free radical polymerizations. One advantage of nitroxide-mediated CRP is that the nitroxide is generally innocuous and can remain in the reaction mix, while other CRP techniques require the removal of the control compounds from the final polymer.

- 5 The mechanism for this control may be represented diagrammatically as below:



with M representing a polymerizable monomer and P representing the growing polymer chain.

- 10 The key to the control is associated with the constants K_{deact}, k_{act} and k_p (T. Fukuda and A. Goto, Macromolecules 1999, 32, pages 618 to 623). If the ratio k_{deact}/k_{act} is too high, the polymerization is blocked, whereas when the ratio k_p/k_{deact} is too high or when the ratio k_{deact}/k_{act} is too low though, the polymerization is uncontrolled.

- 15 It has been found (P. Tordo et al., Polym. Prep. 1997, 38, pages 729 and 730; and C.J. Hawker et al., Polym. mater. Sci. Eng., 1999, 80, pages 90 and 91) that β-substituted alkoxyamines make it possible to initiate and control efficiently the polymerization of several types of monomers, whereas TEMPO-based alkoxyamines [such as (2',2',6',6'-tetramethyl-1'-piperidyloxy-)methylbenzene mentioned in
20 Macromolecules 1996, 29, pages 5245-5254] control only the polymerizations of styrene and styrenic derivatives. TEMPO and TEMPO-based alkoxyamines are not suited to the controlled polymerization of acrylics.

The nitroxide-mediated CRP process is described in, US 6,255,448, US 2002/0040117 and WO 00/71501, incorporated herein by reference. The above-stated patents describe the nitroxide-mediated polymerization by a variety of processes. Each of these processes can be used to synthesize polymers described in the present

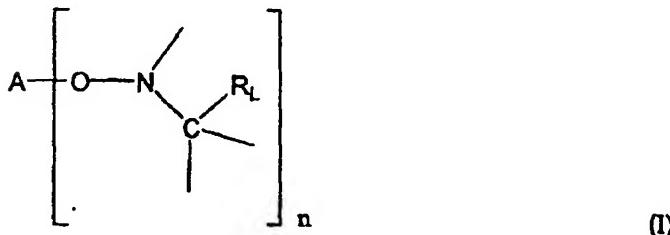
5 invention.

In one process the free radical polymerization or copolymerization is carried-out under the usual conditions for the monomer or monomers under consideration, as known to those skilled in the art, with the difference being that a β -substituted stable free radical is added to the mixture. Depending on the monomer or monomers which

10 it is desired to polymerize, it may be necessary to introduce a traditional free radical initiator into the polymerization mixture as will be evident to those skilled in the art.

Another process describes the polymerization of the monomer or monomers under consideration using a alkoxyamine obtained from β -substituted nitroxides of formula (I) wherein A represents a mono -or polyvalent structure and R_L represents a

15 mole weight of more than 15 and is a monovalent radical, and n ≥ 1.



Another process describes the formation of polyvalent alkoxyamines of formula (I), based on the reaction of multifunctional monomers, such as, but not limited to, acrylate monomers and alkoxyamines at controlled temperatures. The

20 multifunctional alkoxyamines of formula (I), wherein n ≥ 2, may then be utilized to

synthesize star and branched polymeric and copolymeric materials from the monomer or monomers under consideration.

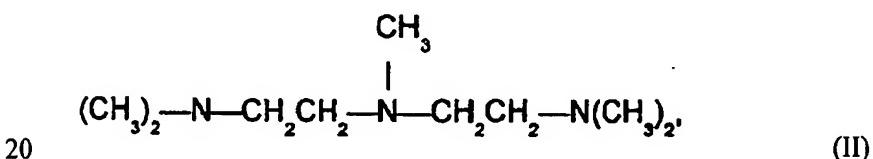
- Another process describes the preparation of multimodal polymers where at least one of the monomers under consideration is subjected to free radical
- 5 polymerization in the presence of several alkoxyamines comprising the sequence of formula (I), wherein n is a non-zero integer and the alkoxyamines exhibit different values of n.

The alkoxyamines and nitroxyls (which nitroxyls may also be prepared by known methods separately from the corresponding alkoxyamine) as described above

10 are well known in the art. Their synthesis is described for example in US Pat. No. 6,255,448 and WO 00/40526.

The polyalkoxyamines of formula (I) may be prepared according to methods known in the literature. The method most commonly used involves the coupling of a carbon-based radical with a nitroxide radical. The coupling may be performed using a

15 halo derivative A(X)_n in the presence of an organometallic system, for instance CuX/ligand (X = Cl or Br) according to a reaction of ATRA (Atom Transfer Radical Addition) type as described by D. Greszta et al. in Macromolecules 1996, 29, 7661-7670. A preferred ligand is - N,N,N',N',N"-pentamethyldiethylenetriamine (PMDETA):



The alkoxyamines of formula (I) according to the present invention may be used for the polymerization and copolymerization of any monomer containing a carbon-carbon double bond, which is capable of undergoing free-radical polymerization. The

polymerization or copolymerization is performed under the usual conditions known to those skilled in the art, taking into account the monomer(s) under consideration. Thus, the polymerization or copolymerization may be performed in bulk, in solution, in emulsion or in suspension, at temperatures ranging from 0 °C to 250°C and preferably ranging from 25°C to 150°C, without any limitation intended by this. Monomers which may be used according to the present invention, mention will be made of vinylaromatic monomers such as styrene, substituted styrenes, dienes, acrylic monomers such as alkyl or aryl acrylates and methacrylates, optionally containing fluorine, for instance methyl acrylate, butyl acrylate or methyl methacrylate, and acrylamides such as N,N-dimethylacrylamide. This method works well for styrenics, acrylates, acrylamides, methacrylates and dienes. Functional monomers, such as epoxy, hydroxy and acid monomers are also easily polymerized by this method.

The alkoxyamines (I) according to the present invention may also be used for the synthesis of "sequenced" block copolymers according to a procedure which consists in carrying out, in a first step, the bulk, solution, suspension or emulsion polymerization of a monomer M1 or a mixture of monomers containing a carbon-carbon double bond capable of undergoing free-radical polymerization in the presence of a alkoxyamine (I) at a temperature ranging from 25°C to 250°C and preferably ranging from 25°C to 150°C, and then, in a second step, allowing the temperature to fall and optionally evaporating off the residual monomer(s), and then, in a third step, introducing the monomer M2 or a new mixture of monomers into the reaction medium obtained above, and then resuming the polymerization by simply raising the temperature.

Polymers made by the nitroxide-mediated process will have nitroxide end groups and the A group from Formula I at the other end or in the center of the

corresponding block. These relatively innocuous nitroxide end-groups can remain on the end of the polymer chains or be removed by an additional processing step.

The nitroxide-mediated polymerization may be used to form block copolymers, which of the present invention are diblock copolymers, triblock 5 copolymers, multiblock copolymers, star polymers, comb polymers, gradient polymers, and other polymers having a blocky structure, which will be known by those skilled in the art. The multiblock and triblock copolymers may consist of two chemically discrete segments, such as in A-B-A triblocks or multiblocks of the formula $(A-B)_n$, where n is > 1 and A and B represent chemically distinct block 10 segments. Or they may contain 3 or more chemically distinct blocks, such as A-B-C triblocks or A-B-C-D multiblock copolymers. The star polymers may contain from 3 to 12 arms, more preferably 3 to 8 and these arms may consist of or diblock, triblock, or multiblock copolymers. These aforementioned structures will be evident to those skilled in the art. Each block segment defined above may consist of a homopolymer, a 15 random copolymer or may be comprised as a gradient copolymer of two or more different monomers.

The block copolymers of the present invention have a controlled molecular weight and molecular weight distribution. Preferably the molecular weight of the copolymer is from 1,000 to 1,000,000 g/mol, and most preferably from 5,000 to 20 300,000 g/mol. The molecular weight distribution, as measured by M_w/M_n or polydispersity is generally less than 4.0, and preferably below 3.0.

One embodiment of the invention is a thickened lubricating oil composition. Uses of such lubricating oils include, but are not limited to motor oils, gear oils, pump 25 oils, turbine oils, hydraulic fluids, cutting fluids and transmission fluids. The block copolymers may be used independently, or as a blend with traditional polymers. In the

lubricating oil composition, a variety of additives may also be present in addition the base oil and polymers mentioned above, including but not limited to detergents, anti-foaming agents, pour point depressants, and anti-corrosion agents.

Due to the control over molecular weight and narrow molecular weight distribution, these polymers exhibit enhanced shear stability. The amphiphilic nature of the block copolymers adds dispersancy to the lubricating oil composition. The incorporation of functional monomers, for instance, but not exclusively, dimethyl amino ethylacrylate, vinyl pyrrolidone, and dimethylacrylamide should further enhance the dispersant nature of these block copolymers. Furthermore, due to the acrylic composition, low molecular weight distribution, amphiphilic nature, and ability to form aggregates in lubricating oils, these polymer should exhibit excellent low temperature properties. These low temperature properties will be evident in SAE J300 Standard viscosity tests, such as cold cranking simulator viscosity (ASTM D5293), scanning Brookfield viscosity (ASTM D 5133), pour point (ASTM D97) and mini-rotary viscosity (ASTM D4684).

The block copolymer is present in a lubricating oil composition at from 0.001 to 40.0 percent by weight, and preferably from 0.01 to 20.0. The level of copolymer used depends on the SAE viscosity grade desired, and the base oils used. One of skill in the art can optimize the SAE grade dependent on the blend of base oils, and the level of copolymer added. Excellent VI improvement has been found using the acrylic copolymers of the present invention. Because of the large VI improvement of these copolymers, oils having a higher VII can be formulated at similar copolymer levels to those currently used, or VI improvement similar to that of currently used VII's can be achieved at lower levels of the copolymer of the invention. While not

being bound by any particular theory, it is believed that the blocky nature of the present copolymers leads to the higher VI improvement.

The lubricating oils of the present invention can be optimized based on several characteristics of the copolymers. These characteristics were tested in Example 3 with 5 the data shown in Table 1. It was found that the total molecular weight of the block copolymer and the composition (i.e., solubility parameter) of the oil-insoluble block had the greatest effect on the VI improvement. Also important was the interaction between the molecular weight and the composition. The weight percent of the insoluble block also had a noticeable effect on the VII. The VII was found to increase 10 as the total Mn increased from 20,000 to 50,000. Changing the insoluble block from polystyrene (a solubility parameter of $18.4 \text{ (J/m}^3\text{)}^{1/2}$) to a poly methyl acrylate block (a solubility parameter of $20.4 \text{ (J/m}^3\text{)}^{1/2}$) also increased the VII. An increase in the weight percentage of the insoluble block also lead to an increase in VII.

Additionally it was found that there was a correlation between the solubility 15 parameter in the insoluble segment and VI improvement, i.e., the larger the difference in solubility parameter, the greater the effect in the VI improvement.

It is anticipated that the resultant amphiphilic character of these materials may also lead to ordered structures such as micelles, which may impart unique properties to the system.

20 While not being bound by any particular theory, it is believed that a critical micelle volume (CMV) occurs in the base oils. At this volume, the divergent viscosity behavior evident in Figure 1 is observed (at about five weight percent of the block copolymer in Figure 1). This level will be dependent on the molecular weight of the copolymer as well as the copolymer composition. It is presumed the amphiphilic 25 nature of the block copolymers will lead to aggregate structures such as micelles

containing an oil-insoluble core and oil-soluble corona. The interaction of and swelling behavior with temperature of these aggregates may lead to predictable viscosity increases and allow for the design of superior viscosity modifiers.

As can be seen in Figure 1 the reduced viscosity of the block copolymer in an oil solution increases linearly with concentration up to 5 percent where the reduced viscosity diverges. This point is very intriguing, as the concentration of block copolymer is proportional to the volume fraction occupied by the polymer in solution. It is presumed the resultant volume fraction will increase with the increasing temperature of the oil due to the enhanced solvation of the polymer chains. The volume fraction increase effect on viscosity is not as significant in the linear region, as compared to the in the divergent region where the behavior is pronounced. From this data, we can presume large viscosity effects (i.e., enhanced VI) can be more readily obtained above a specified volume fraction limit (i.e., divergent point) or critical volume fraction (CVF) value. This behavior could potentially be a powerful tool for tailoring effective VI improvers. Also depicted on the graph are points for a homopolymer of DDMA of similar molecular weight (44,000 g/mol) at 40 and 100 °C. It is clear the divergent behavior is not observed in the homopolymer.

The oil composition of the invention is useful in applications including hydraulic and transmission fluids, gear and motor oils, and oil-based cosmetics and personal care formulations. The block copolymers may be used as pour point depressants. Oil-based cosmetic and personal care formulations benefiting from the thickening imparted by the acrylic block copolymer of the present invention include, for example, toiletries, cleansers, lipsticks, deodorant sticks, nail varnishes, creams, gels and oils, sun creams protective hand creams, night renewal creams, body milks and lotions, light facial creams, protective day creams, liquid moisturizing emulsions,

oil-in-water creams and water-in-oil creams, as well as products for the removal of cosmetic, makeup or personal care products.

The oil compositions of the invention also include oil-based paints, inks, and formulations of pharmaceutical actives.

5

Examples

The controlled architecture block copolymers were synthesized using the following generic protocol. Molecular weights were targeted by manipulating the monomer to initiator concentration ($[M]/[I]$). Therefore a targeted molecular weight 10 could be achieved by setting the $[M]/[I]$ ratio, and then carrying out the polymerization to the desired conversion necessary to reach the target molecular weight. Monomer conversion was conveniently monitored by gas chromatography (GC) analysis or flash devolitization of the monomer under vacuum. The polymer examples were run neat or in solution. Typical solvents used included, toluene, ethyl 15 benzene, and methyl ethyl ketone. Polymerizations were carried out at ambient pressures or run under nitrogen pressure up to 60 psi. Polymerizations were run in standard polymerization vessels both with and without shearing capacity, although adequate mixing capabilities were preferred.

The target block copolymers were prepared by various traditional monomer 20 addition and polymer isolation protocols, as generically described below and will be evident to those skilled in the art, dependant on the desired final block composition. For example, pure block copolymers were prepared by evaporating the residual monomer upon completion of the first block synthesis, subsequently followed by the addition of a second monomer composition different from the first. This second 25 monomer composition then undergoes polymerization. This procedure may be

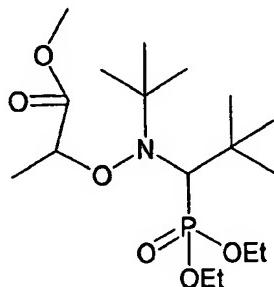
repeated to obtain multiblock copolymers. Gradient block copolymers were synthesized by polymerizing a mixture of two or more monomers. This mixture could result, for instance, by adding a second monomer to the initial polymerization medium prior to evaporation of the residual first monomer, or a multi-monomer mix could be 5 polymerized as a first block, or a multi-monomer mix could be added to an isolated pure first block.

Synthesis of the copolymers of the invention is illustrated by reference to example 1 below. Other copolymers of this invention can be prepared in an analogous manner, as it will be evident to those skilled in the art.

10

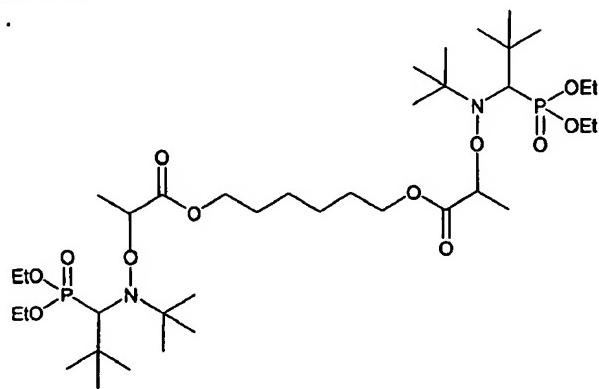
Mono-alkoxyamine initiator

15



20

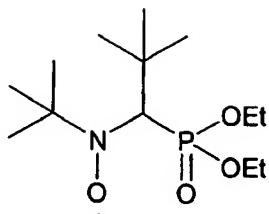
Bis-alkoxyamine initiator



25

Free nitroxide

5



10

Example 1: Polymer synthesis

Example 1: Synthesis of an A-B block copolymer. The A block is polymethyl acrylate (PMA) and the B block is a gradient copolymer of polydodecyl methacrylate and polymethacrylate (PDDMA-*co*-PMA).

- 15 A mixture containing (11.4 grams, 30.0 mmol) mono- alkoxyamine initiator, (0.441 grams, 1.5 mmol) free nitroxide, and (600 grams, 6.97 mol) of methyl acrylate is added to a stainless steel resin kettle under nitrogen (\approx 40 psi), and heated to 110 °C under vigorous stirring. The temperature is maintained for approximately 3 hours, at which point the reaction had reached 50% conversion as measured by GC. The
- 20 reaction mixture is then cooled to room temperature. The M_w = 12,600 g/mol, and M_n = 10,300 g/mol as determined by SEC analysis and referenced to polystyrene standards. In a glass reactor equipped with a condenser, 40.5 grams (159.4 mmol) of dodecyl methacrylate is heated to 100°C under a nitrogen atmosphere and vigorous stirring. To 25.3 grams of the PMA polymer and monomer mixture from above, 2.18
- 25 grams (25.3 mmol) of methyl acrylate was added. The resultant polymer mixture

(12.65 grams of PMA and 14.83 grams of methyl acrylate) is added to the DDMA monomer over 1 minute. The resulting mixture is cloudy as the PMA is not completely soluble in the dodecyl methacrylate and methyl acrylate monomer solution. The temperature is held at 100-105°C and the cloudy mixture becomes clear

5 in the first 30 minutes, indicating the formation of a block copolymer is occurring and the resultant block acts as a stabilizer for the corresponding mixture. The reaction is run until approximately 60% monomer conversion is achieved as monitored by GC. The reaction takes several hours when an acrylate monomer is present, however if only a methacrylate is present the polymerization is generally done in less than 1

10 hour. The resultant viscous liquid was diluted by an equal volume of THF, and the solution was precipitated into cold stirring methanol. The $M_w = 56,500$ g/mol, and $M_n = 39,600$ g/mol as determined by SEC analysis compared to polystyrene standards.

15 Example 1-1: PMA-b-PDDMA

An analogous A-B block copolymer was prepared in which the A block is polymethyl acrylate (PMA) and the B block is a pure block of polydodecyl methacrylate (PDDMA). The residual monomer from the first block PMA from example 1 was removed. The neat PMA was then dissolved in toluene (approximately 20 equal weight) prior to adding to the heated lauryl methacrylate monomer solution. This protocol resulted in a pure block copolymer of PMA and PDDMA.

Examples 1-A to 1-P

The following polymers were prepared in accordance with the procedures
25 given above for Example 1 and 1-1. Homopolymers and diblocks were synthesized

with the monoalkoxyamine initiator, while triblocks were synthesized with the difunctional alkoxyamine initiator. Mn and PDI values listed are based on SEC analysis as compared to polystyrene standards and the relative wgt % of monomers listed are based on conversions by GC or ^1H NMR analysis.

- 5 For the following examples, “co-“ will represent a copolymer, and “b-“ will represent a block.

Example 1-A (Comparative): Polyethylhexyl acrylate (PEHA) homopolymer, Mn = 26 kg/mol and PDI = 1.4.

- Example 1-B (Comparative): PEHA -co-polystyrene (PS), Mn = 49.5 kg/mol, PDI = 10 1.5, and PS = 50 wgt %.

Example 1-C: Polydodecyl methacrylate (PDDMA)-b-PS, 28.0 kg/mol, PDI = 1.6, and PS = 16 wgt %.

Example 1-D: PDDMA-b-PS-b-PDDMA, 31.6 kg/mol, PDI = 1.7, and PS = 35 wgt %.

- 15 Example 1-E: PDDMA-co-PS-b-PS-b-PS-co-PDDMA, 31.6 kg/mol, PDI = 1.7, and PS = 48 wgt %.

Example 1-F: PDDMA-b-PMA-b-PDDMA, 23.0 kg/mol, PDI = 1.5, and PMA = 48 wgt %.

- 20 Example 1-G: PDDMA-co-PEHA-co-PS, 25.6 kg/mol, PDI = 1.8, and PDDMA = 64 wgt %, PEHA = 24 wgt%.

Example 1-H: PDDMA-b-poly *n*-butylacrylate(PnBA)-b-PDDMA, 77.6 kg/mol, PDI = 1.8, and PnBA = 65 wgt %.

Example 1-I: PDDMA-b-PMA-b-PDDMA, 76.0 kg/mol, PDI = 2.0, and PMA = 60 wgt %.

- 25 Example 1-J: Polymethoxy ethyl acylate (PMEA)-b-PDDMA.

Example 1-K: PDDMA-b-PMEA-b-PDDMA.

Example 1-L: polyethyl acrylate (PEA)-b-PDDMA.

Example 1-M: PDDMA-b-PEA-b-PDDMA.

Example 1-N: Polydimethyl acrylamide (PDMAA)-co-PEA-b-PDDMA.

5 Example 1-O: Polydimethyl amino ethyl acrylate (PDMAEA)-co-PEA-b-PDDMA.

Example 1-P: Poly(polyethylene glycol methoxy ether) acrylate (PEGME)-co-PEA-b-PDDMA.

Example 2: Testing of polymers

10 Polymers 1A, 1B, 1C, 1D, 1H, and 1I of Example 1 were dissolved in a light paraffinic mineral oil (Base oil 1) at the listed percentages. Polymers 1E, 1F, and 1G of Example 1 were dissolved in a 150 N base oil from TOTAL (Base oil 2) at the listed percentages. The viscosity of each lubricating oil composition was measured at both 40°C and at 100°C by ASTM standard D445. The resultant VI was calculated
15 using ASTM D2270. The results are found in Table 1 below.

TABLE 1

SAMPLE	WT % In Oil	40°C Visc. Cs	100°C Visc. Cs	VI
Base Oil 1	---	36	6.0	110.2
Base Oil 2	---	31.5	5.3	101.2
1A	5	43.9	7.3	128.7
1B	5	Not Soluble	Not Soluble	---
1C	5	58.7	9.2	137.5
1D	5	51.9	9.2	159.8
1E	5	49.3	8.8	158.1
1F	5	62.9	10.7	160.2
1F	7.5	96.6	18.1	207.8
1G	5	43.1	7.0	121.5
1G	10	81.3	12.8	157.4
1H	2.5	50.4	8.7	149.3
1H	5	89.1	16.0	192.3
1H	10	267.2	49.0	245.2
II	5	45.9	9.5	197.7

Example 3: Optimization of VI improvement

5 Sixteen well-defined block copolymer compositions were synthesized by using either a mono alkoxyamine or a difunctional alkoxyamine. These 16 compositions were a part of an experimental design investigation. The five variables investigated in the experimental design were; the solubility of the insoluble segment or monomer composition (from slightly insoluble to highly insoluble in oil or PS

versus PMA), wt% of the insoluble segment, total M_n of the block copolymer, wgt % gradient of insoluble component, and block architecture (diblock vs. triblock).

These 16 polymers were characterized, tested, and a comprehensive data analysis packet was compiled. The packet contains the following information for each composition:

1. SEC data (for both the 1st block (PMA or PS) and each corresponding final di or triblock copolymer) to determine the M_n, PDI, and confirm the absence of “dead” first block chains or confirm the “livingness” of the polymerization.
- 10 2. Liquid absorption chromatography (LAC) data to determine the presence of homopolymer contamination.
3. ¹H NMR to determine the relative weight percent polydodecyl methacrylate (PDDMA) in each sample.
- 15 4. The kinematic viscosity of each sample was acquired at both 40 and 100 °C by ASTM standard D445 and the corresponding VI calculated (by using ASTM D2270).

A summary of these results is depicted in Table 2 below. Not included in table 1 is the LAC data. This data indicated less than 5 wgt% homopolymer was present in each composition, confirming the “livingness” of the system.

20 The first column indicates the sample #. Columns 2-6 indicate the targeted experimental design parameters (M_n total, insoluble segment, weight percent insoluble block, gradient %, and block type (triblock (3) or diblock (2)).

DDMA was used as the soluble segment in each polymer and the viscosity measurements were obtained on 5 wgt % polymer solutions in 150N base oil received from TOTAL.

Table 2

Run	Mn total	Insoluble monomer	Wt% Insol.	Grad- ient %	Block Type	Mn Insol. kg/mol	Mn 2 nd	% DDMA NMR	Visc 40 C cst	Visc 100 C cst	VI
1	50	MA	50	0	2	22.2	42.8	69	180.72	37.17	255
2	50	MA	20	0	3	12.3	35	78	213.23	40.43	244
3	50	PS	20	25	3	11.6	28.4	59	69.84	10.82	144
4	50	PS	50	25	2	21.2	28.9	49	105.12	17.6	181
5	20	MA	50	0	3	11	12	52	62.9	10.66	160
6	50	PS	50	0	3	24.8	21.1	56	61.27	10.88	171
7	50	MA	20	25	2	111	35.3	69	198.49	49.23	301
8	20	PS	50	0	2	9.2	8.8	43	46.69	7.71	133
9	50	PS	20	0	2	10	26.1	77	89.8	10.82	102
10	20	MA	20	25	3	4	18	73	47.93	8.2	145
11	20	PS	50	25	3	10.9	14.2	39	43.28	8.02	160
12	20	PS	20	25	2	4.5	23.5	60	53	8.63	139
13	20	MA	50	25	2	10.3	9.7	48	52.33	9.31	162
14	20	PS	20	0	3	5.5	14.3	68	46.9	7.76	134
15	20	MA	20	0	2	4.4	13.6	77	63.37	10.28	150
16	50	MA	50	25	3	24.9	28.1	58	97.4	20.86	241

- Example 4: Starting with a multifunctional alkoxyamine (Formula I where n>2) and
- 5 proceeding with the polymerization procedures described in example 1, star block copolymers were synthesized. The multifunctional acrylates were formed by adding a slight molar excess (of amino-alkoxyamine to unsaturated groups in the multifunctional acrylate) of a mono-alkoxyamine of Formula I where n=1, to a multifunctional acrylate at 60 °C for < 1 hour (ethanol is used as a solvent). The
- 10 monoalkoxyamine is chosen such that the dissociation temperature is < 60 °C.

Example 5: Sample number 7 and number 16 from Table 2 would be blended at 1 weight percent and at 5 weight percent in a typical base oil supplied from TOTAL

such as 100N or 150N base oil stock. These polymers would be expected to display excellent pour point, shear stability, and low temperature behavior. These characteristics would be seen through test results from SAE J300 Standard viscosity tests, such as cold cranking simulator viscosity (ASTM D5293), scanning Brookfield viscosity (ASTM D 5133), pour point (ASTM D97) and mini-rotary viscosity (ASTM D4684).

10 Example 5-A: The polymerization of methyl acrylate is carried out directly in a paraffinic mineral oil, using a mono-alkoxyamine and the standard polymerization conditions from example 1. After several hours, PDDMA was added to the polymerization mixture. The corresponding PMA-b-PMA-co-PDDMA polymer was left in the oil solution

15 Example 5-B: The solution from Example 5-A is diluted with a base oil from TOTAL and used directly as a VII and pour point depressant.

20 Example 5-C: The polymerization mixture obtained in Example 5-A is treated with a traditional free radical initiator, to react or (chase) the residual DDMA and MA monomers.

Example 5-D: The solution from 5-C is diluted with a base oil from TOTAL and used directly as a VII and pour point depressant.

25 Example 5-E: Example 1-N is added at 1% to a base oil from TOTAL and used as a dispersant.

Example 5-F: Example 1-O is added at 1% to a base oil from TOTAL and used as a dispersant.

Example 5-G: sample 16 from Table 1 is added at 1% to an aviation hydraulic fluid and utilized as a VII with excellent shear stability.

Example 5-H: sample 16 from Table 1 is added at 1% to a multigrade hydraulic fluid and utilized as a VII with excellent shear stability.

Example 6 Experiment that yielded Figures 1 and 2

5

- The DDMA homopolymer was synthesized using a monoalkoxyamine and has a Mn = 44.5 kg/mol and PDI = 2.2. The block copolymer (PMA-b-PDDMA) has an Mn = 23 kg/mol and PDI = 1.6. The wgt % PDDMA is 52 %. The aforementioned block copolymer and PDDMA homopolymers were dissolved in a 150N base oil 10 supplied by TOTAL. The reduced viscosity of these solutions at various polymer concentrations have been plotted at both 40 and 100 °C. Evident from this plot is the unique behavior of the block copolymer as compared to the analogous homopolymer. Without being bound to any particular theory, it is believed the amphiphilic nature of the acrylic block is responsible for the unique behavior demonstrated by Figure 1. 15 This behavior leads to the excellent VII behavior demonstrated by the block copolymer as compared to the corresponding homopolymer.

Example 7

- The same experiment performed in Example 6 was repeated using a block 20 copolymer having nearly twice the molecular weight (Mn 46.4 kg/mol, PDI = 2.0 and 76.7 wgt % PDDMA). The results are shown in Figures 2. As expected the divergent point was shifted to a much lower polymer concentration, due to the increased 25 molecular weight and therefore increased volume fraction of the solution occupied by polymer. Again as the critical volume fraction or CVF is reached, a divergent behavior is observed. This CVF has a consequential affect on the VI, which is more pronounced in the block copolymer case than observed for simple homopolymers or

random copolymers. The diblock reaches the divergence point at a lower concentration (approximately 3 wgt %), and this in-turn has a strong influence on the resultant VI as can be seen in both Figures 3 and 4. These figures are plots of VI vs wgt % polymer. Figure 4 has simply been rescaled (omits the 10 wt% block data point) for clarity. As expected, there is a large increase in the VI as we increase the amount of block copolymer in solution. The homopolymer VI also increases with concentration, however it begins to level-off at higher concentrations. The block copolymer shows a more aggressive behavior as the VI increases rapidly with increasing concentration and the increase is more pronounced at higher concentrations. This data indicates a significant cost/performance may be realized with these types of block structures. This is clearly seen in Figure 4 in which the VI for the 3 wgt% block copolymer is equal to the VI for 15% homopolymer.

15

What is claimed is:

1. A thickened oil composition comprising
 - a) from 99.999 to 60 weight percent of one or more oils; and
 - b) from 0.001 to 40 weight percent of a controlled free-radical acrylic block copolymer having at least one acrylic block.
- 5 2. The thickened oil composition of claim 1 comprising from 0.01 to 20 weight percent of said controlled free-radical acrylic block copolymer.
3. The thickened oil composition of claim 1 wherein said oil composition is a
10 lubricating oil composition.
4. The thickened oil composition of claim 1 wherein said controlled free-radical acrylic block copolymer is an amphiphilic block copolymer
5. The thickened oil of claim 4 wherein said amphiphilic block copolymer comprises:
 - 15 1) at least one oil-soluble polymer block having a solubility parameter of from 14 to 18 (J/m^3)^{1/2}; and
 - 2) at least one non-oil soluble polymer block having a solubility parameter of greater 18 (J/m^3)^{1/2}.
6. The thickened oil composition of claim 5 wherein said non-oil soluble block has
20 a solubility parameter of greater than 20 (J/m^3)^{1/2}.
7. The thickened oil of claim 1 wherein said acrylic block copolymer is formed by a nitroxide-mediated polymerization process.
8. The thickened oil of claim 1 wherein said acrylic block polymer is formed from all acrylic monomers.

9. The thickened oil of claim 1 wherein said non-oil soluble polymer block comprises poly(methyl acrylate) or polystyrene.
10. The thickened oil composition of claim 1, wherein said acrylic block copolymer comprises micelles of block copolymers.
- 5 11. The thickened oil composition of claim 2 wherein said oil composition has a VII of greater than 150.
12. The thickened oil composition of claim 9 wherein said VII is greater than 200.
13. The thickened oil composition of claim 10 wherein said VII is greater than 250.
- 10 14. The thickened oil of claim 1 wherein said oil composition comprises a hydraulic fluid, a transmission fluid, a gear oil, a motor oil, a cosmetic formulation, or a personal care formulation.
15. The thickened oil of claim 1 wherein said acrylic block comprises at least 90 mole percent of one or more acrylic monomers.
- 15 16. The thickened oil of claim 1 wherein said acrylic block comprises at least 95 mole percent of one or more acrylic monomers.
17. The thickened oil composition of claim 3 further comprising detergents, anti-foaming agents, pour point depressants, and anti-corrosion agents.
18. The thickened oil composition of claim 1 wherein said acrylic block copolymer is 20 multifunctional.

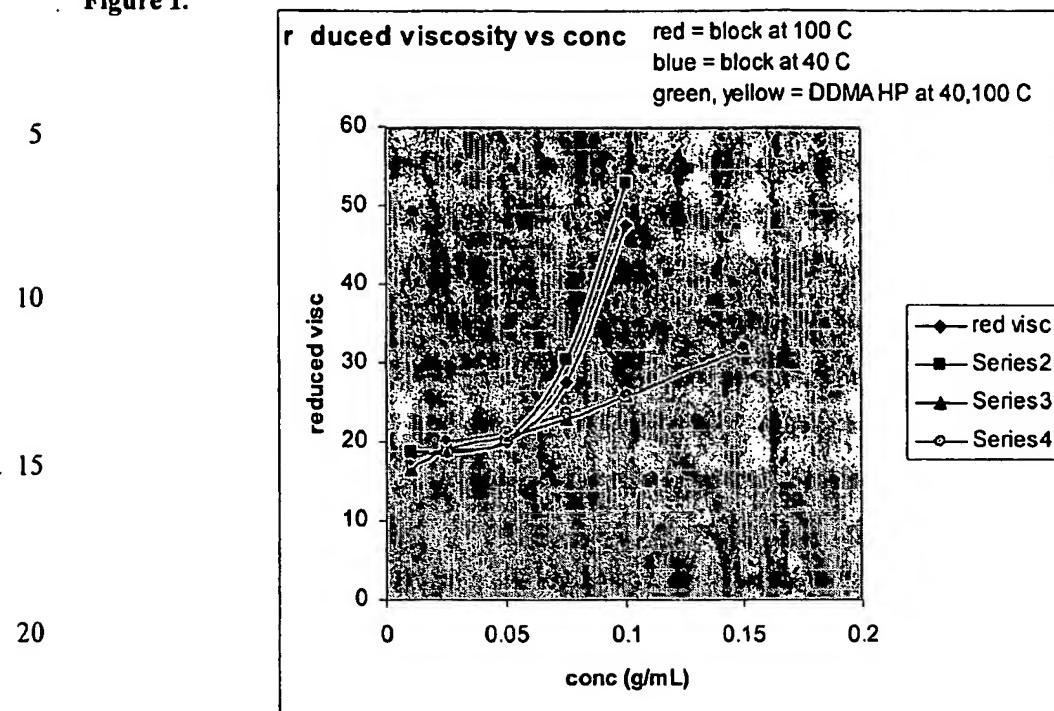
ABSTRACT

The present invention relates to acrylic block copolymers synthesized by a controlled free-radical process, and their use as thickeners in oil-based compositions.

- 5 The acrylic copolymers are especially useful as viscosity index improvers in lubricating oil.

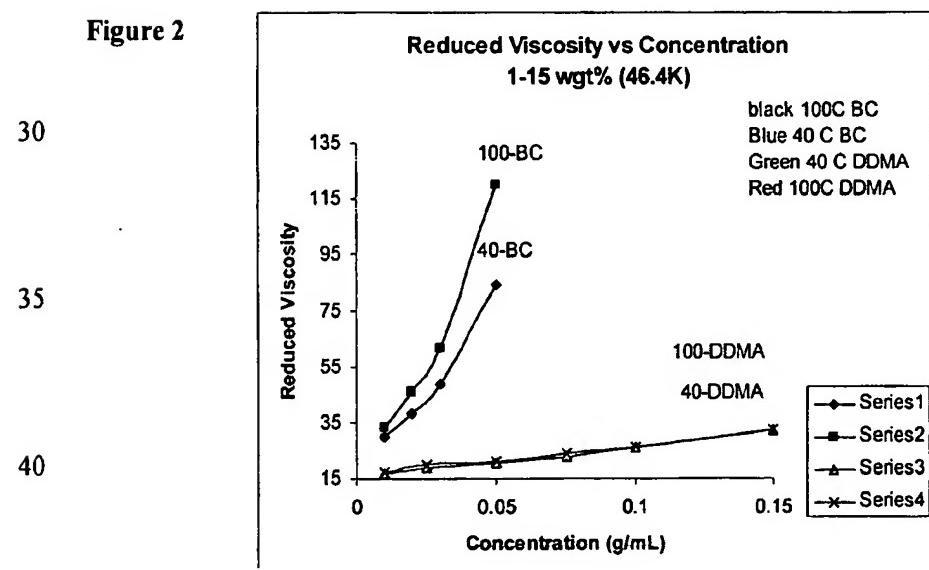
10

Figure 1.



25

Figure 2



45

50

Figure 3

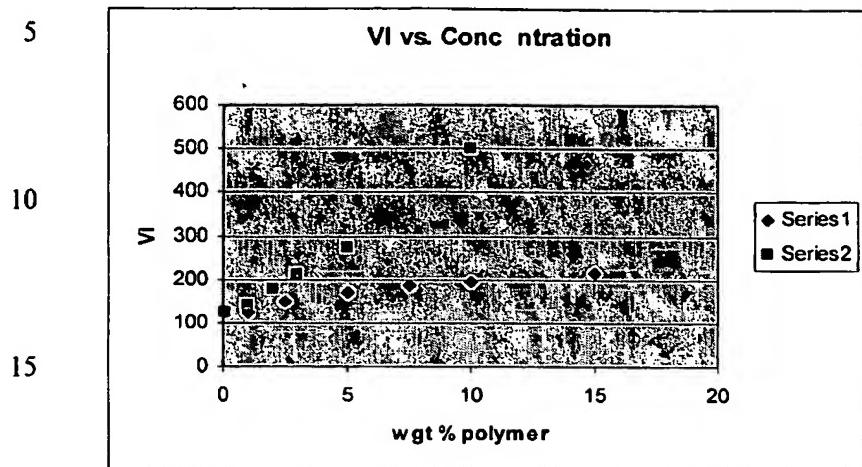
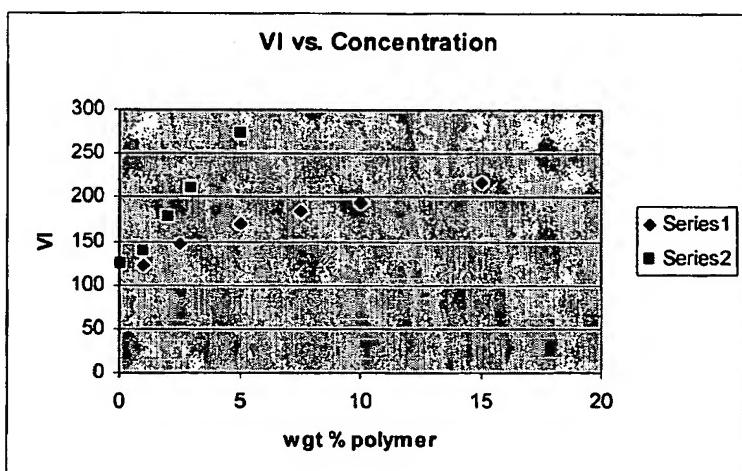


Figure 4



Document made available under the Patent Cooperation Treaty (PCT)

International application number: PCT/US04/034236

International filing date: 15 October 2004 (15.10.2004)

Document type: Certified copy of priority document

Document details: Country/Office: US
Number: 60/525,549
Filing date: 26 November 2003 (26.11.2003)

Date of receipt at the International Bureau: 17 December 2004 (17.12.2004)

Remark: Priority document submitted or transmitted to the International Bureau in compliance with Rule 17.1(a) or (b)



World Intellectual Property Organization (WIPO) - Geneva, Switzerland
Organisation Mondiale de la Propriété Intellectuelle (OMPI) - Genève, Suisse